

Tanzania

Petroleum (Conservation) Act

## Petroleum (Interim) Regulations, 2000

Government Notice 297 of 2000

Legislation as at 31 July 2002

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Petroleum (Interim) Regulations, 2000 (Government Notice 297 of 2000)  
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# Tanzania

## Petroleum (Conservation) Act

# Petroleum (Interim) Regulations, 2000

## Government Notice 297 of 2000

Published in Tanzania Government Gazette

**Commenced on 1 December 1999**

*[This is the version of this document at 31 July 2002.]*

*[Note: This legislation was revised and consolidated as at 31 July 2002 and 30 November 2019 by the Attorney General's Office, in compliance with the Laws Revision Act No. 7 of 1994, the Revised Laws and Annual Revision Act (Chapter 356 (R.L.)), and the Interpretation of Laws and General Clauses Act No. 30 of 1972. All subsequent amendments have been researched and applied by Laws.Africa for TANZLLI.]*

*[Section 25; G.N. No. 297 of 2000]*

## Part I – Preliminary provisions (regs 1-2)

### 1. Citation

These Regulations may be cited as the Petroleum (Interim) Regulations.

### 2. Interpretation

In these Regulations unless the context requires otherwise—

"**Act**" means the Petroleum (Conservation) Act<sup>1</sup>;

"**Commissioner**" means Commissioner responsible for petroleum;

"**Company**" means a company incorporated under the Companies Ordinance<sup>2</sup>;

"**petroleum**" shall have the meaning assigned to it in section 3 of the Act;

"**product specifications**" means petroleum products specification provided in the Schedule to these Regulations;

"**qualified oil company**" means any of the oil marketing companies which have been granted permission by Minister responsible for petroleum in accordance with the Act, to carry out the business of procuring, transporting, storing, distributing and selling petroleum products in mainland Tanzania;

"**Tipper**" means Tanzania and Italia Petroleum Refining Company Limited, a limited liability company incorporated under the Companies Act with its principal offices located in Dar es Salaam, Tanzania<sup>3</sup>;

1

[Cap. 392](#)

2

[Cap. 212](#)

3

[Cap. 212](#)

"**Technical Task Force**" means a task force appointed by the Minister responsible for petroleum with the basic functions to regulate, monitor and to oversee the procurement, transportation, storage, distribution and pricing of petroleum products in the country.

## **Part II – Establishment of technical task force committee (regs 3-7)**

### **3. Establishment**

There is hereby established a Technical Task Force Committee to act as an interim petroleum regulatory body.

### **4. Constitution**

The Commissioner shall be the Chairman of Technical Task Force and the Minister shall appoint the members not exceeding seven who shall also include members with experience and knowledge in petroleum matters.

### **5. Functions**

The functions of the Technical Task Force shall be—

- (a) to determine, in consultation with qualified oil companies the country's requirements of petroleum products;
- (b) to monitor supplies of petroleum imported for consumption in the country;
- (c) to enforce compliance of the provisions of these Regulations;
- (d) to advise the Minister on the status of supplies of petroleum in the country, quality of petroleum, pricing and other matters as may be necessary to ensure a reliable supply of petroleum in the country;
- (e) to monitor the procurement, transportation, storage and distribution of petroleum in the country;
- (f) to collect, store and furnish the Minister with information from qualified oil companies and from other sources on imports, deliveries, storage, distribution, pricing and other relevant information on petroleum; and
- (g) to advice on the specification of petroleum to be used in the country.

### **6. Meetings**

The Committee shall meet as and when it deems necessary to accomplish its tasks.

### **7. Eligibility**

- (1) The qualified oil companies shall be the only bodies eligible for marketing petroleum in the country on such terms and conditions the Tasks Force shall prescribe.

## **Part III – Importation of petroleum (regs 8-12)**

### **8. Importation procedure**

- (1) The importation of petroleum shall be—
  - (a) made from a supply source which generate competitive prices for the country;

- (b) received in a bonded warehouse or such other appropriate receiving facilities as may be advised by the Customs Department; and
- (c) inspected by an authorised surveyor appointed by the Bank of Tanzania who shall inspect all imports of petroleum and issue a certificate available to all relevant authorities including the Technical Task Force for the purposes of verifying quantities, quality and cost of the import.

## 9. Companies to submit information on petroleum

All qualified oil companies shall submit to Technical Task Force—

- (a) schedule of import quantities and estimated delivery time for each import;
- (b) stock positions of petroleum from all depots in the country on a weekly basis;
- (c) sales of petroleum by type of product and by regions on a monthly basis;
- (d) the retail price for each product in all regional headquarters in the country every time they revise their petroleum product prices;
- (e) information on the change of shareholding of the company, change of name, which might assist the Technical Task Force in monitoring the supply arrangement of petroleum in the country; and
- (f) on a quarterly basis, progress reports on investment programmes if any.

## 10. Product quality

All petroleum products entering the domestic market shall conform to specifications provided in Schedule to these Regulations.

## 11. Offences and penalties

Any person who contravenes any provisions of these Regulations commits an offence and upon conviction is liable to a fine not exceeding one hundred thousand shillings or to imprisonment for a period not exceeding three years or both, the fine and imprisonment.

## 12. Application specification to the petroleum products

The specifications set out in the Schedule to these Regulations shall be applicable to the petroleum products purchased or supplied in the country.

### Schedule

#### Product specifications

##### 1. Premium motor gasoline (leaded)

Specified Gravity at 20%	gr/ml.	0.742	0.75	ASTMD 1298
Octane No. research method				
Lead Content	gr.Pb/AG		max. 95	ASTMD 2699

Distillation				ASTMD 86
• 10% Evaporated to				
• 50%Evaporatedto				
• 90%Evaporatedto	°C	60	max. 71	
• 20% minus 10% Evaporated to	°C	100	max. 115	
• End Point	°C	155	max. 180	
• Residue				
• R. V. P. at 100°C	°C	8	min. 8	
	°C	180	max. 205	
	% Vol	1	max. 2	
	p.s.i.a.	7.7	max. 9	ASTMD 323
Existent Gum	Mg/100ml	1	max. 4	ASTMD 381
Induction Period		240	min. 240	ASTMD 525
Sulphur Content	%wt	0.019	max. 02	ASTMD 1266
Copper Strip Corrosion (3hr. at 212 °F)	No. strip	1 strip	max. 1	ASTMD 130
Mercaptan Sulphur	%wt	NIL	max. 0.0015	ASTMD 1323
Colour		Red		Visual
Dye Content Red	Gr/100AG	0.5		Visual
Odour		Marketable		

**2. Motor premium gasoline (unleaded)**

PRODUCT CHARACTERISTIC	UNIT MEASURE	AVERAGE VALUE	MIN/MAX VALUE	ANALYTICAL METHOD
Specific Gravity at 20%	°C	0.742	0.75	ASTMD 1298

Octane No. research method	-	max. 95	ASTMD 2699	
Lead Content	Gr.Pb/AG	max. 0.013	ASTMD 526	
Distillation:	ASTMD 86			
• 10% Evaporated to	°C	60	max. 71	
• 50%Evaporated to	°C	100	max. 115	
• 90%Evaporated to	°C	100	max. 180	
• 20% minus 10% Evaporated to	°C	8		
• End Point	°C	8		
• Residue	%wt	0.9	max. 1	
	%Vol	1	max. 2	
R. V. P. at 100°C	p.s.i.a.	7.7	max. 9	ASTMD 323
Existent Gum	Mg/100ml.	1	max. 4	ASTMD 381
Induction Period		240	min. 240	ASTMD 525
Sulphur content	%wt	0.019	max. 0.2	ASTMD 1266
Copper Strip Corrosion (3hr. at 212 °F)	No/strip	1/strip	max. 1	ASTMD 130
Mercaptan Sulphur	%wt	Nil	max. 0.0015	ASTMD 1323
Colour		Red		Visual
Dye Content Red	Gr/100/AG	0.5		Visual
Odour		Marketable		

### 3. Automotive gasoil

PRODUCT CHARACTERISTIC	UNIT MEASURE	AVERAGE VALUE	MIN/MAX VALUE	ANALYTICAL METHOD
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Specific Gravity at 20°C	-	0.845	min. 0.82 max. 0.87	ASTMD 1298
Colour ASTM	-	0.5	max. 3.5	ASTMD 1500
Cetane Index (calc.)	-	55	min. 52	ASTMD 976
Viscosity kinematic @ 100°F	cSt	3.6	min. 1.6	ASTMD 445
Cloud Point	°C	-3	max. -4.5	ASTMD 2500
Sulphur Content	%wt	0.9	max. 1	ASTMD 130
Copper Strip Corrosion (Three hours 212°F)	No. strip	1 -Strip	max. 1	ASTMD 130
Carbon Residue (on 10% Bottoms)	%wt	0.02	max. 0.15	ASTMD 189
Water	%Vol	Nil	max. 0.05	ASTMD 95
Sediment	%wt	TRACES	max. 0.05	ASTMD 473
Ash	%wt	TRACES	max 0.01	ASTMD 482
Neutralisation Value—				
- Strong Acid Number	Mg.KOH/gm	0.03	max. 1	ASTMD 664
- Total	Mg/KOH/mg	0.03	max. 1	
Flash Point (PMCC)	°C	96	min. 70	ASTMD 93
Distillation—	%Vol	95	min. 90	
- Recovery at 367°C				
Calorific Value	BTU/lb.	19,200		

#### 4. Liquid petroleum gas

PRODUCT CHARACTERISTIC	UNIT MEASURE	AVERAGE VALUE	MIN/MAX VALUE	ANALYTICAL METHOD
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Specific Gravity at 60/60°F	Gr/ml/	0.5518	max. 0.575	ASTMD 1298
Vapour Pressure at 100°F	p.s.i.g	92.5	max. 100	ASTMD 1267
Volatile Sulphur(On unstenched product)	Gr/100 cu.ft.	NIL	max. 0.25	ASTMD 1226
Copper Strip Corrosion	No. Strip	1 Strip	max. 1	ASTMD 1830
Composition (Chromatographic analysis)				ASTMD 2163
- Hydrocarbon C2	%Vol	NIL	max. 1	
- Hydrocarbon C3 plus C4	%Vol	100	min. 97.5	
Hydro Carbon C5	% Vol	NIL	max. 1.5	
Odouriser R. S. H.			min. 1	

#### 5. Fuel oil (furnace oil)

PRODUCT CHARACTERISTIC	UNIT MEASURE	AVERAGE VALUE	MIN/MAX VALUE	ANALYTICAL METHOD
Specific Gravity at 60/60 °F	-	0.9415	max. 0.99	ASTMD 1298
Viscosity Redwood 1 @ 100 °F	Sec	1000	max. 1000	IP. 70
Calorific Value (Gross)	BTU/lb.	18,625	min. 18,300	
Sulphur Content	%wt	2.4	max. 3.5	ASTMD 1552
Water	%Vol	TRACE	max. 0.75	ASTMD 95
Sediment	%wt	TRACE	max. 0.15	ASTMD 473
Neutralisation—				ASTMD 664
Strong Acid Number	Mg.KOH/gm	NIL		

Flash Point (PMCC)	°C	95	min. 70	ASTMD 93
Fluidity @ 32 °F		PASS		
Explosivity	%wt	50	max. 50	F.S.1151
Pour Point	°C	+ 10	+ 20 min	ASTMD 97
Ash	%wt	TRACE	max. 0.1	ASTMD 482
Carbon Residue Conradson	%wt	7	max. 11	ASTMD 189

#### 6. Industrial diesel fuel (ido)

PRODUCT CHARACTERISTIC	UNIT MEASURE	AVERAGE VALUE	MIN/MAX VALUE	ANALYTICAL METHOD
Specific Gravity at 60/60 °F	-	0.85	max. 0.92	ASTMD 1298
Diesel index	-	56	min. 45	ASTMD
Kinematic Viscosity @ 100 °F	cSt	5	max. 8	ASTMD 445
Calorific value (Gross)	BTU/lb	19,350	min. 19,250	
Sulphur Content	%wt	1.2	min. 1.5	ASTMD 1552
Carbon residue - Conradson	%wt	0.25	max. 0.45	ASTMD 189
Water	%wt	TRACES	max. 0.25	ASTMD 95
Sediments	%wt	TRACES	max. 0.02	ASTMD 473
Ash	%wt	TRACES	max. 0.02	ASTMD 482
Asphaltenes	%wt	0.3	max. 0.5	IP 143
Neutralisation:—				ASTMD 974
- Strong Act Number	mg./KOH/gm	NIL		

- Total Acid Number	mg./KOH/gm	0.03	max. 1	
Flash Point (PMCC)	°C	105	min. 70	ASTMD 93
Pour Point	°C	-4	max. 4.5	ASTMD 97

#### 7. Illuminating kerosene

PRODUCT CHARACTERISTIC	UNIT MEASURE	AVERAGE VALUE	MIN/MAX VALUE	ANALYTICAL METHOD
Specific Gravity 60/60 °F	-	0.792	0.82	ASTMD 1298
Colour Saybolt	-	+30	min. 20	ASTMD 156
Smoke Point	mm	26	min. 24	ASTMD 1322
Char Value	mg/kg	14	max. 20	IP 10
Distillation:				ASTMD 86
- Recovery at 200 °C	% Vol	60	min. 20	
- End point	°C	240	min. 300	
Flash Point Abel	°F	113	min. 100	IP 170
Sulphur Content	%wt	0.0003	max. 0.2	ASTMD 1266
Copper Strip Corrosion	No. Strip	1 -Strip	max. 1	ASTMD 130
Odour		Marketable		
Calorific Value	BTU/lb	20,000		

#### 8. Aviation turbine fuel

PRODUCT CHARACTERISTIC	UNIT MEASURE	AVERAGE VALUE	MIN/MAX VALUE	ANALYTICAL METHOD

Specific Gravity at 60/60 °F	-	0.795	min. 0.775	ASTMD 1298
Colour Saybolt	-		min. 20	ASTMD 156
Calorific value	BTU/lb	18,600	min. 18,400	ASTMD 240
Aniline Gravity product				ASTMD 611/1298
Distillation:				ASTMD 86
• I. B. P	°C	156	max. 165	
• 20%Evaporated to	°C	185	max. 200	
• 50%Evaporated to	°C	198	max. 232	
• 90%Evaporated to	°C	220	max. 260	
• End Point	°C	238	max. 288	
• Residue	%Vol	1	max. 1.5	
• Loss	%Vol	0.5	max. 1.5	
Viscosity at 0 °F	cSt	8	max. 6	ASTMD 445
Viscosity at minus 39°F	cSt	5	max. 15	ASTMD 445
Flash point - Abel	°F	240	max. 100	IP. 170
Flash Point	°F	max. 150	ASTMD 56	
Sulphur Content	%wt	0.0002	max. 0.2	ASTMD 1266
Mercaptan Sulphur	%wt	NIL	max. 0.001	ASTMD 1219
Doctor Test		NEGATIVE		ASTMD 464
Copper Strip Corrosion (2 hrs. at 122 °F)	No. Strip	1 -Strip	max. 1	ASTMD 130
Existent Gum (Steam jet)	Mg/100	1	max. 7	ASTMD 381

Aromatic Content	%Vol	16.9	max. 20	ASTMD 1319
Freezing point	°C	-53	max. 50	ASTMD 2386
Strong Acid Number	Mg.KOH/gm	NIL		ASTMD 974
Total Acid Number	Mg.KOH/mg	0.005	max. 0.012	ASTMD 974

**9. Jet ai/dpk**

The aviation fuel quality requirements for the current jointly operated system (AFQRJOS) for jet A-1 present the most stringent requirements of the following three specifications:

- (a) British Ministry of Defence Standard Def Stan 91.91/Issue 2 (DERD 2994) OF 8th March, 1996 for turbine fuel, aviation "Kerosene Type", Jet A-I, Nato Code F-35, joint Service designation AVTUR.
- (b) Astm Standard Specification D L655-95 for aviation turbine fuels "Jet A-I".
- (c) International Air Transport Association (IATA) guidance material for aviation turbine fuels, 2nd edition, dated December, 1994 for "Kerosine Type fuel".

Jet fuel which meets the AFQRJOS is usually referred to as jet A-I to checklist, or checklist jet A-I and definition, meets all three of the above specifications.

The AFQRJOS Joint fuelling system checklist for Jet A-I is defined in the following table which should be read in conjunction with the remarks attached to the table to this document.

JOINT FUELLING CHECK LIST FOR JET A. 1	
	Issue 17 - October, 1998
	Supersedes Issue 16 June 1996.

Embodying the most stringent requirements in the following specifications for the grade shown:

- (a) British MoD DEF STAN 91-91/Issue 2 dated 8th May, 1996 (plus all amendments up to 3 dated 11th September, 1998), Jet A-I.
- (b) ASTM D 1655-97, Jet A-I.
- (c) IATA guidance Material for Aviation Turbine Fuels, 3rd Edition, March 1998, Kerosene Type Fuel.

PROPERTY	LIMITS	TEST	METHOD	REMARKS	
APPEARANCE	Clear, bright and visually free from solid matter and undissolved water at normal ambient temperature	IP	ASTM		
COMPOSITION				See 1	
Total Acidity, mg	max 0.015	354	D3242		
KOG/g					
Aromatics, %vol	max 22.0	156		D1319	
OR				D1319	
Aromatics, %vol	25.0	156		D3701 or	
AND hydrogen					
Content, % mass	Report	338		D3343	
Sulphur Total %					
mass	max 0.030		107	D1266 or D4294 or	
Sulphur Mercaptan					
% mass	0.0030	342	D2622	D1552	
OR Doctor Test	Negative	30	D3227		
Hydroprocessed					
Fuel in batch,					
% vol	Report (Inc. nil or 100%)		D4952	See 2See 3	

<b>VOLATILITY</b>					
Distillation		123	D86		
Initial Boiling Point,		Report			
deg C					
Fuel Recovered	max	205			
10% vol. at °C					
50% vol. at °C	max	Report			
90% vol. at °C		Report			
End Point, °C	max	300			
Residue, %vol	max	1.5			
Loss, %vol	max	1.5			
Flash Point, °C	min	38			
Density at 15°C kg/ m <sup>3</sup>	775-840	170 or 303	D1298 or D4052	See 4	
<b>FLUIDITY</b>					
Freezing Point,	max	minus 47	16	D2386	Or D5901 or D4305 (See 5)
Viscosity at 20°C	max	8.0	71	D445	Or D5972
<b>COMBUSTION</b>					
Specific Energy,					
net MJ/kg	min	42.8	381	D4809	See 6

Smoke Point, mm	min	25	D1322		
OR					
Luminometer					
Number OR	min	45		D1740	
Smoke Point, mm	min	19		D1322	
AND Naphthalenes,					
%vol	max	3.0		D1840	
<b>CORROSION</b>					
Corrosion, Copper					
Classification (2h at 100°C)		1	154	D130	
Corrosion, Silver,					
Classification (4h at 50°C)		2	227		
<b>STABILITY</b>					
Thermal Stability	25.0		232	D3241	
(JFTOT)					
Control Temp 260°C					
Filter Pressure					
different, mm Hg	max	Less than 3 'Peacock'			



Tube Deposit					
Rating (Visual)	max	'Abnormal'			
		colour deposits			
<b>CONTAMINANTS</b>					
Existent gum,	max	7	131	D381	
mg/100ml					
Water Reaction					
Interface Rating	max	lb	289	D1094	
Microseparometer					
(MSEP), rating					
Fuel with Static					
Dissipator Additive	min	70		D3748	
OR					
Fuel without Static					
Dissipator Additive	min	85			
<b>CONDUCTIVITY</b>					
Electrical					
Conductivity, Ps/m		50-450	274	D2624	See 8
<b>ADDITIVES (only</b>					
those additives					

approved in DEFSTAN					
91-91/2 are permitted)					
Antioxidant, mg/L					
in Hydroprocessed and Synthetic Fuels	max	24.0 17.0-24.0			See 9
(Mandatory) in Non-hydroprocessed					
Fuels (Optional)	max	24.0			
Metal					
Deactivator,					
Mg/L (Optional)	max	5.7			See 10
Static dissipator,					
Mandatory), mg/L	max	3.0			
First Doping Stadis					
450					
Re-dopingSee Notes 11		1.0			See 11

Antioxidants are mandatory in hydroprocessed fuels and must be added immediately after processing.	Corrosion inhibitor/lubricity improver is not permitted unless agreed by all the participants in a joint system.
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The types and concentration of all additives used, including "nil" additions, are to be shown on refinery Certificates of Quality and other documents.

See also Note 12 for information on fuel lubricity. Fuel System Icing Inhibitor is not permitted unless agreed by all the participants in a joint system.

### Main Table Remarks

1. Attention is drawn to Amendment 3 (11 September, 1998) of DEF STAN 91-91 which approves the Semi-Synthetic Jet Fuel (SSJF) produced by SASOL Oil under approval reference FS (Air) SSJET/1. For SSJF additional testing requirements apply and reference should be made to the Amendment. As a result of this change, this particular semisynthetic fuel meets the requirement of this Check List.
2. The Doctor Test is an alternative requirement to the Sulphur Mercaptan Content. In the event of conflict between the Sulphur Mercaptan and Doctor Test results, the Sulphur Mercaptan shall prevail.
3. The need to report the %vol. of hydroprocessed fuel (including "nil" or "100%" as appropriate) on refinery Certificates of Quality for Jet A-I to check List derives from Annexes A. 1.1 to A.1.1 to A.1.3 in DEF STAN 91.91/2 about antioxidant additives (additive dose rate cannot be interpreted unless the proportion of hydroprocessed fuel is known Recipients of Jet A-I cannot check or demonstrate that fuel complies with checklist if the information is omitted from refinery Certificates of Quality. Note that "hydroprocessed" includes hydrotreated, hydrofined and hydrocracked. A refinery blending Jet A-I batches from more than one of these processes should report one (total) hydroprocessed % vol. on Certificates of Quality.
4. Subject to a minimum of 40 deg C, results obtained by method ASTM D56(Tag) may be accepted.
5. See footnotes in individual specifications for viscosity limitations on the use of ASTM D4305.
6. Calculated specific energy by one of the following methods is acceptable: ASTM D3338 or ASTM D4529/IP 381.
7. Naphthalenes content by method ASTM D1840 must be obtained using the solvent iso-octane.
8. MSEP is required only in DEF STAN 91.91/2. Note 7 of that specification states "These MSEP requirements apply only at point of manufacture. No precision data are available for fuels containing SDA; if MSEP testing is carried out during downstream distribution no specification limits apply and the results are not be used as the sole reason for the rejection of a fuel fuel".
9. Conductivity limits apply at the point, time and temperature of delivery to the user.
10. Approved antioxidant additives are listed in Annex A. 1.4 of DEF STAN 91.91/2, together with appropriate RDEA/A/-Qualification Reference for quoting on refinery Certificate of Quality.
11. The approved Metal Deactivator Additive (MDA) appears in Annex A. 2. 2 of DEF STAN 91.91/2. See also Annex A. 2.1. about the need to report thermal stability before and after using MDA to improve this property when contamination of Jet A-I by any of the trace metals listed in Annex is unproven.
12. Although ASA-3 is out of production, a Note in Annex-A. 3.3.2 of DEFSTAN 91-91/2 permits the use of residual stocks, provided that their quality and effectiveness remains satisfactory.
13. Re-doping limits for Static Dissipator additives are—

Same additive:		max. mg/L
Cumulative concentration	Stadis 450(RDE/A/621)	5.0

Change of additive or original additive not known	Stadis 450 (RDE/A/621)	2.0
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14. For important advisory information on the lubricity of aviation turbine fuels see Annex B of DEF STAN 91.91/2.